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DEPENDENCE OF VANADIUM RECOVERY ON OXIDATION STATE IN ITS SOLVENT EXTRACTION FROM HYDROCHLORIC ACID SOLUTIONS WITH TRI N BUTYL PHOSPHATE

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ABSTRACT

The recovery of vanadium as V(V), VO_2^+ and V(IV), VO^{2+} from diluted and concentrated HCl solutions by trinn-butyl phosphate (TBP) dissolved in n-hexane has been independently studied.

The oxidation state of the vanadium species was found to have a profound effect on the percentage vanadium extraction (E%).

At the pH range of 0.2-2.0, both V(V) and V(IV) were poorly extracted, with an optimum E% = 6.0 and 1.0 for V(V) and V(IV) respectively. However, at an optimum 6M HCl concentration, V(V) has a remarkable E% = 81.4 which was 2.0% for V(IV) and with both not much affected by temperature variation.

The extraction equilibrium constant, K_{ex} , was 1.52, and 0.02 for V(V) and V(IV) respectively.

Based on slope analysis, electronic and infrared spectra data, the organic extracts of V (V) and V(IV) complexes were formulated as $VO_2Cl(TBP)_2$. 2HCl and $VOCl_2$ (H₂O)(TBP) respectively. The study reveals that V(V) is much better recovered than V(IV) from HCl solutions by TBP, and which might be informative in hydrometallurgical separation processes.

Keywords: Vanadium; Recovery; Oxidation State; TBP; Spectra

INTRODUCTION

The use of solvent extraction to recover economic minerals from lean ores has continued to generate waves of interest over the past few decades. Since vanadium is a component of various steels employed in machine parts and construction equipments (Greenwood and Earnshaw, 1997), the study of its extraction process deserves the attendant attraction in hydrometallurgy.

Both V(V) (cationic and anionic) and V(IV) (cationic) are extractable as neutral complexes into organic diluents but with varying quantitative extractions (Ritcey and Ashbrook, 1984). The DAPEX process (Agers *et al.*, 1962) extracts V(V) as VO_2^+ , and V(IV) as VO^{2+} with di (2- ethylhexyl) phosphoric acid (D2EHPA) and with kinetics of the former in D2EHPA n-hexane thoroughly investigated (Ipinmoroti and Hughes, 1990). Some workers (Thomas et al., 2003) studied the extraction of V(V) from HCl solutions with tri-nbutyl phosphate (TBP) in kerosene diluent and reported the extraction constants and isotherms. The extraction of complexes of anionic vanadium (VO₃) with tri-n-octylmethylammonium chloride (TOMAC) has been extensively investigated (Hirai and Kosamawa, 1990; Hirai et a.l, 1993).

Other researchers (Nasu *et al.*, 1999) have reported a comparative study of the relative extraction of iron as Fe (II) and Fe (III) from thiocyanate solutions but little effort has hitherto been made to address the relative extractions of V(V) and V(IV) under the same extraction conditions such as acid medium, extractant and diluent.

Since the relative quantitative extractions of V(V) and V(IV) from HCl solutions by TBP in n-hexane has not been much studied, it is hence thought worthwhile initiating independent studies on the species with a view of exploiting it later for a large-scale vanadium processing or separation processes where vanadium is a contaminant. However, the choice of the vanadium species would depend among other things on whether the vanadium is to be recovered from the acid leach or retained. In the present work, the extraction of V(V) and V(IV) from HCl solutions with TBP in n-hexane highlighting the dependence of vanadium extraction on the oxidation state is presented.

MATERIALS AND METHODS

The chemicals, NH₄VO₃, HCl, KCl, ascorbic acid, n-hexane, TBP, D2EHPA were obtained from the

British Drug House Limited (BDH). All the chemicals were of analytical grade except TBP and D2EHPA and were used without further purification.

Preparation of 0.05 MVO₂⁺ Stock Solutions

Ammonium metavanadate (5.85 g, 0.05 mol) was dissolved in various concentrations of hydrochloric acid (1.0-6.0 M), followed by the addition of KCl (7.48 g, 0.1mol) and finally made up to the 1 litre mark. The adjustment of pH was effected by adding NaOH or HCl and subsequently measured by the pH meter.

Preparation of 0.05 M VO²⁺ Stock Solutions

To the stock solution of V(V) prepared above was added ascorbic acid (19.11 g, 0.11 mol) with the solution turning to blue. The amount of vanadium (IV) present was determined (Ipinmoroti, 1981) by titrating with 0.02 M KMnO₄ at 60^oC. The reduction was complete in all the solutions.

Extraction and Analytical Procedure

Different concentrations of TBP and TBP-D2EHPA mixtures were prepared by mixing appropriate amounts of the extractants with n-hexane. 15 cm³ portions of TBP or mixed extractants were equilibrated separately with 15 cm³ portions of V(V) and V(IV) solutions as the case may be at the appropriate pH and temperature in a separating funnel, swirled manually and later on a mechanical shaker operated at 120 rpm for 2 minutes (found optimum for equilibration). The

layers were allowed to separate out, the lower aqueous layer ran into a conical flask and the upper organic layer removed from the top of the separating funnel to avoid contamination. The amount of metal extracted was determined by spectrophotometer, BIOCHROM 4060 model, by measuring the absorbance of the pink complex formed between vanadium and 3% H₂O₂ in a 2.0 M H₂SO₄ medium at 450 nm. The infrared and electronic spectra were recorded on an infrared spectrophotometer, BUCK SCIENTIFIC M O D E L and ultraviolet-visible spectrophotometer respectively.

RESULTS

Figure 1 shows the effect of pH on percentage V(V) and V(IV) extraction. Both oxidation states are lowly extracted between pH of 0.2 and 2.0. Studies have been limited to this range to avoid hydrolysis for which the species are known (Sato, 1979). V(V) has higher percentage extraction (E% = 6.0) at a pH of 0.2 and subsequently decreased to E% = 4.03 at a pH of 0.4 which later remained constant thoughout, while for vanadium (IV) the percentage extraction was constant (E% = 1.0) throughout the pH range of study.

Fig. 2 shows the effect of increase in HCl concentration on the percentage V(V) and V(IV) extraction. The percentage V(V) extraction varies



FIg.1: Effect of pH on Percentage V(V) and V(IV) Extraction from HCl solution [V(V)] = 0.05 M; [V (IV)] = 0.05 M; [TBP] = 1.098 M; [KCI] = 0.1 M



[V(V)]; [V(IV)] 0.05 M; [TBP] = 1.098 M; [KCI] = 0.1 M

Table 1: Effect of Initial Vanadium (V) and (IV) Concentration on the Distribution Co-efficient and Percentage Extraction of Vanadium (V) and (IV) [TBP] = 1.098M (30% v/v); [KCl] = 0.1M, [HCl] = 6M

	V(V)		V(IV))
Conc	D	E	D	Ε
(M)		(%)		(%)
0.01	3.348	77.00	0.010	1.00
0.02	3.651	78.50	0.010	1.00
0.03	3.615	78.33	0.010	1.00
0.04	4.000	80.00	0.010	1.00
0.05	4.376	81.40	0.01	1.00

from 6.0% for 1.0 M HCl to 80.0% for 6.0 M HCl. In the case of V(IV), increase in HCl concentration had no effect on the percentage vanadium extraction as it remained constant at 2.0% throughout the concentration range and further works were therefore done at 6.0 M HCl.

Table 1 shows the effect of initial V(V)and V(IV) concentrations on percentage extraction. The percentage V(V) and V(IV)extractions were nearly constant when the initial V(V) and V(IV) concentrations were varied between 0.01 and 0.05 M. However, the concentration of 0.05 M where E% = 81.4 for V(V) and E% = 1.0 for V(IV) was used throughout the work.

The effect of TBP concentration on the percentage V(V) and V(IV) extraction is presented in Figure 3. The percentage vanadium (V) extraction reached a peak of E% = 81.4 at 1.1 M (30%v/v) TBP concentration and subsequently decreased, while the percentage V(IV) extraction (Figure 3) was nearly constant (E% = 1.0-1.96) when the TBP concentration was varied in the range 0.37-1.47 M.

Ojo et al.: Dependence of Vanadium Recovery







Fig 4: Effect of the Addition of D2EHPA to TBP on Percentage V(V) Extraction from HCI Solution [V(V)] =0.05 M; [HCI] = 6.0 M; [TBP] = 1.098 M

Table 2: Effect of Variation in Temperature on Percentage V(V) and V(IV) Extraction from 6.0 M HCl Solution with TBP. [V(V)], [V(IV)] = 0.05 M; [KCl] = 0.1 M; [TBP] = 1.098 M

	V(V)		V(IV)	
	D	E	D	E
Temp. (K)		(%)		(%)
301	4.376	81.40	0.01	1.00
306	4.556	82.00	0.01	1.00
311	4.556	82.00	0.01	1.00
316	4.556	82.00	0.02	1.96
321	4.556	82.00	0.110	9.90

Ojo et al.: Dependence of Vanadium Recovery **Table 3:** The Electronic Spectra data (cm⁻¹) and Assignments for the Complexes

Compound	ບ/ cm⁻¹	ε/M ⁻¹ cm ⁻¹	Probable Assignment
V(V) COMPLEX	30303	68	Charge transfer
	23529	22	
V(IV) COMPLEX	31250	1250	Charge transfer
	15152	1100	d – d allowed transition

Table 4: The Infrared Spectra Data (cm⁻¹) and Assignments for TBP and Complexes

1277vs	v(P = O)
1028vs	$\upsilon(P-O-C)$
2882w	υ(H - Cl)
1270s	$\upsilon(P = O)$
1034vs	v(P - O - C)
980w	υ (V-Cl)
960w	$\upsilon(V = O)$
1269s	v(P = O)
1027vs	υ(P – O– C)
980w	υ (V-Cl)
857w	$\upsilon(V = O)$
	1277vs 1028vs 2882w 1270s 1034vs 980w 960w 1269s 1027vs 980w 857w

vs = very strong; s = strong; w = weak.

The effect of the addition of D2EHPA (0.29 0.86 M) to 1.1 M TBP is presented in Figure 4.

The effect of temperature on the percentage vanadium (V) and IV) extraction was investigated in the range 301-321 K and presented in Table 2.

It was observed that increase in temperature had no significant effect on V(V) extraction as the percentage extraction was nearly constant throughout; but in the case of V(IV) a slight increase in percentage extraction was observed (E % = 1.0 at 301 K and E% = 9.9 at 321 K). The electronic spectra for TBP extracts of V(V) and V(IV) are shown in Table 3 while the i.r. spectra of the free TBP ligand and vanadium TBP extracts of V(V) are shown in Table 4.

DISCUSSION OF RESULTS Effect of pH

The poor extraction of both vanadium (V) and (IV) at the pH range 0.2 - 2.0 could be explained on the basis of low concentration of H⁺ which could have helped in removing coordinated water molecules from the complex as solvated ion needed for high extractability.

Effect of HCl Concentration

The observed high percentage V(V) extraction compared with V(IV), with increased HCl concentration (Figure 2) might be due to the fact that $V0_2^+$ is easily neutralized by the Cl counter-ion, more available at high acid concentrations or forms a more stable complex than VO²⁺ and this trend we have found agrees quite well with previous works done in CCl₄ (Tedesco and Rumi, 1978) and benzene (Sato, 1979) diluents with TBP as extractant. This position is further strengthened by the fact that no appreciable change in percentage extraction of V(V) and V(IV) was observed with pH variation.

Effect of TBP Concentration

With V (V), the initial increase in E% with increase in TBP concentration, was due to availability of more extractant molecules needed for solvation of the neutral complex thereby enhancing higher solubility and extractability in the organic phase (Ritcey and Ashbrook, 1984) while the decrease in E% at higher TBP concentration might be due to a hindrance in the diffusion of the molecules of the solvated complex through the interfacial zone as a result of steric factor.

Since TBP extracts metals by solvation, the number of solvated TBP molecules, x, depends among many other things, on the coordination number of central atom, and the nature of the diluent (Ritcey and Ashbrook, 1984; Sato *et al.*, 1980). If the extraction of VO_2^+ into TBP can be expressed by equation 1,

 $VO_{2(aq)}^{+} + CI_{(aq)}^{+} + xTBP_{(org)}^{-} = VO_{2}CI. XTBP_{(org)}^{-}(1)$ Then the equilibrium constant is given by $K = [VO_{2}CI. xTBP]$ (2)

$$K_{ex} = \begin{bmatrix} VO_{2}CI, XTBP \end{bmatrix}_{org}^{x}$$

$$\begin{bmatrix} VO_{2}^{+} \end{bmatrix}_{aq} \begin{bmatrix} CI \end{bmatrix}_{aq} \begin{bmatrix} TBP \end{bmatrix}_{org}^{x}$$

$$K_{ex} = D$$

$$\begin{bmatrix} CI \end{bmatrix}_{aq} \begin{bmatrix} TBP \end{bmatrix}_{org}^{x}$$
(3)

Where 'aq' and 'org' represent aqueous and organic phases respectively, and the distribution coefficient, D is given by the ratio of the analytical concentration of VO_2^+ in the organic and aqueous phases.

At constant [Cl], Equation (3) reduces to:

$$K_{ex} = \underline{D}$$

$$[TBP]_{org}^{x} \qquad (4)$$
i.e. $D = K_{ex}[TBP]_{org}^{x} \qquad (5)$
hence,

 $\log D = x \log [TBP]_{org} + \log K_{ex}$

It is therefore expected that a log - log plot of D against TBP concentration as shown in Figure 5, should yield a straight line with the slope equal to 'x', the number of TBP molecules (Forrest, 1969) solvated during VO_2^+ extraction. From the slope, x = 2.3, thus suggesting two as the possible solvation number for VO_2^+ extraction from acid-chloride medium into n-hexane and was found to agree with previous work done in kerosene

(6)



FIG 5: A Log-log plot of Distribution Coefficient Against TBP Concentration for V (V)

(Thomas et al., 2003).

The value of $K_{ex} = 1.52$

For V(IV) extraction (Fig. 3) the percentage vanadium extraction varies from E% = 1.0 at 0.37 M (10% v/v) TBP, to 1.96 at 1.47 M (40% v/v) TBP and the relevant scheme for extraction would be according to Equation 7.

 $\text{VOCl}_{2(aq)} + n \text{TBP}_{(org)} \hookrightarrow \text{VOCl}_2.n \text{TBP}_{(org)}(7)$

where 'n' is the number of solvated TBP molecules.

Like the case of V(V) above, Equation 6 would express the distribution coefficient of V(IV).

Therefore, a log log plot of D against TBP

concentration (Fig. 6) would yield a slope equal to 'n'

The value of 'n' was found to be 0.86 suggesting that one TBP molecule is solvated to a vanadyl ion. The value of $K_{ex} = 0.02$

The values of K_{ex} for V(V) and V(IV) differs almost by a factor of 100 indicating that the extraction of V(V) is more favoured than V(IV).

Effect of the addition of D2EHPA to 1.098M TBP on V(V) Extraction.

The addition of D2EHPA to 1.1 M TBP (Figure 4) produced an initial slight increase from E% = 81.4 to E% = 86.0 perhaps due to a solvating behaviour of D2EHPA, but further



FIG. 6: A Log-log plot of Distribution Coefficient Against TBP Concentration for V (IV)

additions translated to a decrease from E% = 81.4 to E% = 74.0 which might be ascribed to increased interaction between the TBP and D2EHPA via hydrogen bonding (Brunette *et al.*, 1979). The addition of D2EHPA could therefore be viewed as having an unappreciable effect on V(V) extraction by TBP. Since there was insignificant extraction of V(IV) by TBP, no attempt was made to further investigate the effect of the addition of D2EHPA.

Effect of Temperature

The unappreciable increase in percentage extraction when the temperature was increased (Table 2) might point to an overall mass transfer of vanadium being dependent on a diffusioncontrolled process, as increase in temperature is supposed to increase the vanadium extraction if chemically controlled, moreso that it is not exothermic.

Electronic and Infrared Spectra

V(V) shows absorptions (Table 3) at 30303cm⁻¹ (325 nm) and 23529 cm⁻¹ (425 nm) ascribed to ligand-metal charge transfer (LMCT) since V(V) has a d° electronic configuration.

V(IV) shows weak absorptions (Table 3) at 31250 cm⁻¹ (320 nm) and 15152 (660 nm) ascribed to charge transfer and d-d allowed transition respectively and both with surprisingly high molar extinction coefficient arising from a departure from octahedral geometry to a C_{4v} symmetry (Sato, 1979 & Ojo, 2003).

The bands (Table 4) at 1277 and 1028 cm⁻¹ assigned to (P = O) and (P-O-C) vibrations respectively, shift to 1270 and 1034 cm⁻¹ in the complex, indicating the involvement of the phosphoryl group in coordination. The new but weak bands at 960 and 980 cm⁻¹ assigned to (V = 0) and (V Cl) respectively, conclusively confirm the coordination of vanadium to TBP. And finally the band observed at 2882cm⁻¹ absent in the

ligand has been assigned to (H-Cl) vibration (Barrow, 1983), this band is absent in V(IV).

In the V(IV) complex, the (P = O), (P O - C) and (V = O) bands are observed at 1269, 1027 and 857 cm⁻¹ respectively, and are similar to that of previous workers(Zhang *et al.*, 1996; Remya & Reddy, 2004). The (V = O) for V(IV) was much lower than V(V) probably due to the later exhibiting a more hard acid effect on the vanadyl bond. The possibility of the extracted [VOCl₂(H₂O)TBP] complex hydrolyzing to form species such as [VO(OH)Cl.TBP] and [VO(OH)Cl.TBP]₂ could not be ruled out as expressed by Equation 8.

 $VO^{2+} + H_2O \leftrightarrows VO(OH)^+ + H^+$

where the hydrolysis constant of 10⁻⁶ has been established (Sato, 1979) even though a magnetic moment data might be needed to confirm a dimerised structure.

(8)

From the foregoing, the extracted complexes of V(V) and V(IV) have been formulated as $[VO_2Cl(TBP)_2].2HCl$ and $[VOCl_2TBP(H_2O)]$ respectively, with the following proposed structures (Figs. 7 and 8):

CONCLUSIONS

It could be concluded from the present study that if vanadium is to be recovered from hydrochloric acid leach it would fair better if processed as V(V), VO_2^+ than V(IV), VO^{2+} , but if it is to be retained in the acid leach during







Figure 8: The Proposed Structure of V(IV) TBP Complex, [VOCl₂TBP(H₂O)] separation from other metals, then V(IV), VO^{2+} is the viable alternative.

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Ife Journal of Science Tables of Contents: June Edition 2011; Vol. 13, No. 1

Omotoye Olorode, Sekinat O. Hassan, Olajumoke A. Olabinjo and Idris O. Raimi	Tithonia (Asteraceae) in Nigeria	I
Obuotor E.; Adewumi A. A. and Olaleye V. F.	The Effect of Copper on Some Laboratory Indices of Clarias Gariepinus (Burchell 1822).	П
Salami, B. M. Conte, R. A. and Falebita, D. E.	Geoelectric Evalution of the Groundwater Potential of Parts of Osogbo, Southwestern, Nigeria	17
Ogunfowokan A.O., Akanni M.S., Ajibola R.O and Ayinde F.O.	Trophic Status and Physico-Chemical Parameters of Three Reservoirs in Osun State Nigeria	27
Oláyíwolá M.A ¹ and Odébòdé M.O.	Foraminiferal Distribution of Southwestern Nigeria's Offshore Littoral Sediments: Benthic Faunal Diversity Indices and Patterns	45
Chinedu S.N., Okochi V. I. and Omidiji O.	Cellulase Production by Wild Strains of Aspergillus Niger, Penicillium Chrysogenum and Trichoderma Harzianum Grown on Waste Cellulosic Materials.	57
Bayode S. and Akpoarebe O.	An Integrated Geophysical Investigation of a Spring in Ibuji, Igbara-Oke, Southwestern Nigeria.	63
M. O. Adepoju and J. A. Adekoya	Reconnaissance Geochemical Study of a Part of Igarra Schist Belt, Southwestern Nigeria	75
Adesina, G.O., Akinyemiju, O.A. and Muoghalu, J.I.	Checklist of the Aquatic Macrophytes of Jebba Lake, Nigeria	93
Fasasi, K. A., Malaka, S. L. O. and Amund, O. O.	Studies on the Life Cycle and Morphometrics of Honeybees, Apis Mellifera Adansonii (Hymenoptera: Apidae) In A Mangrove Area of Lagos, Nigeria.	103
A.O. Olorunfemi, K.S. Salahudeen and T.A. Adesiyan	Ground Water Quality in Ejigbo Town and Environs, Southwestern Nigeria	111
Govardhan Singh, R.S; Ogunsina, B.S. and Radha, C.	Protein Extractability from Defatted <i>Moringa Oleifera</i> Lam. Seeds Flour	121
A. M. A. Sakpere	Identification of ISSR Primers for Genetic Analysis of <i>Telfairia</i> Occidentalis Hook F.	129
O. K. Owoade, F. S. Olise, H. B. Olaniyi, I. B. Obioh and E. Bolzacchini	Mass and Energy Audit in a Nigerian Iron and Steel Smelting Factory: An Operational and Efficiency Study.	133
F. A. Oloyede, B. Aponjolosun & A. A. Ogunwole	Reproductive Potentials of a Tropical Fern <i>Cyclosorus Afer</i> (Christ.) Ching (Thelypteridaceae: Pteridopyhte) at Obafemi Awolowo University, Ile Ife, Nigeria	143
M.O.Olawole, L. Msimanga, S.A.Adegboyega & F.A. Adesina	Monitoring and Assessing Urban Encroachment into Agricultural Land - A Remote Sensing and GIS Based Study of Harare, Zimbabwe	149
Benjamin, U.K and Nwachukwu, J.I	Model Compaction Equation for Hydrostatic Sandstones of the Niger Delta.	161
J.O. Ojo and C.E. Adeeyinwo	Dependence of Vanadium Recovery on Oxidation State in its Solvent Extraction from Hydrochloric Acid Solutions With TRI N Butyl Phosphate	175
Akintorinwa, O. J., Ojo J. S. and Olorunfemi M. O.	Appraisal of the Causes of Pavement Failure along the Ilesa - Akure Highway, Southwestern Nigeria Using Remotely Sensed and Geotechnical Data	185
O. J. Matthew and O. O. Jegede	Modelling Soil Surface Temperature and Heat Flux Using Force-Restore Method at an Agricultural Site in Ile-Ife, Nigeria.	199
Ojo J.F.	On the Theory of One Dimensional Integrated Autoregressive Bilinear Time Series Modelling	209